

Environmental Research and Education Foundation

# Leachate 201 Treatment Issues/Challenges



# Course Overview

- Review of Leachate 101
- Leachate 201
  - Considerations for Disposal
  - Off-site Disposal - Issues for POTWs
  - Leachate Treatment Technologies & Application
  - Emerging Issues





# Review of Leachate 101

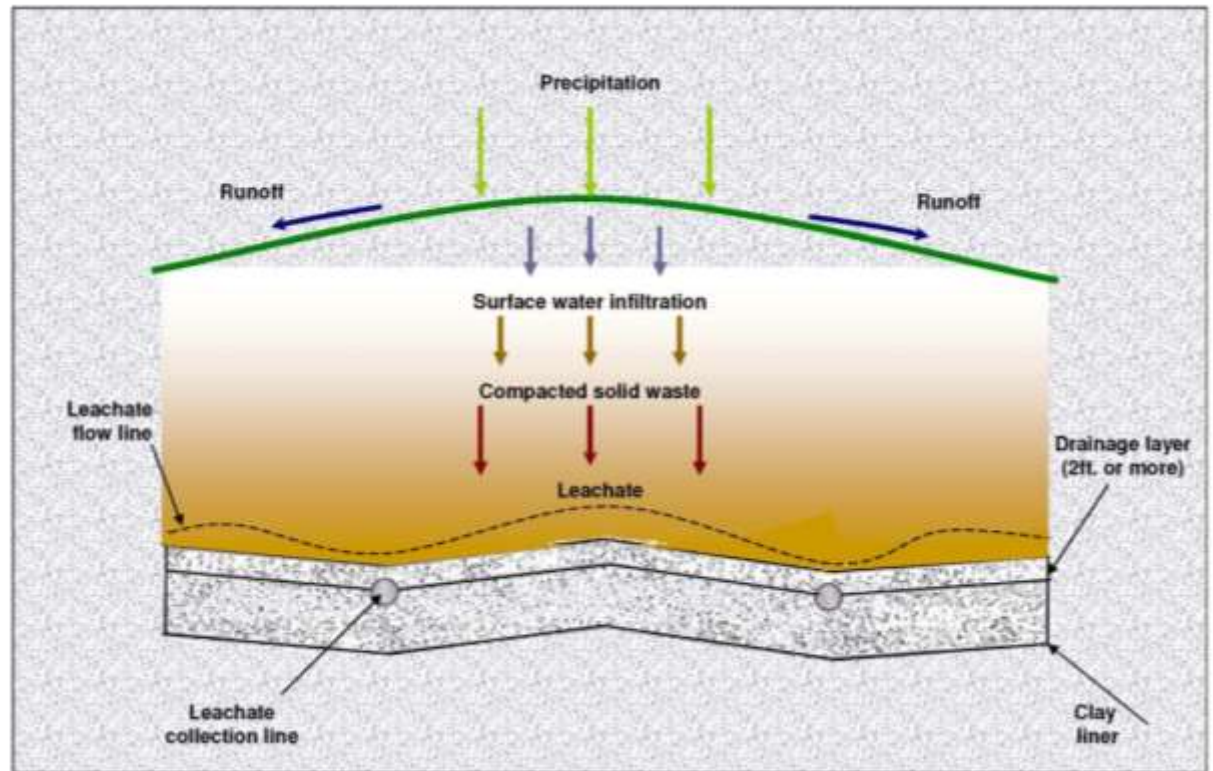
# General Concepts Covered

- 1 Leachate generation
- 2 Leachate Composition
- 3 Impacts of climate on leachate
- 4 Management and Storage



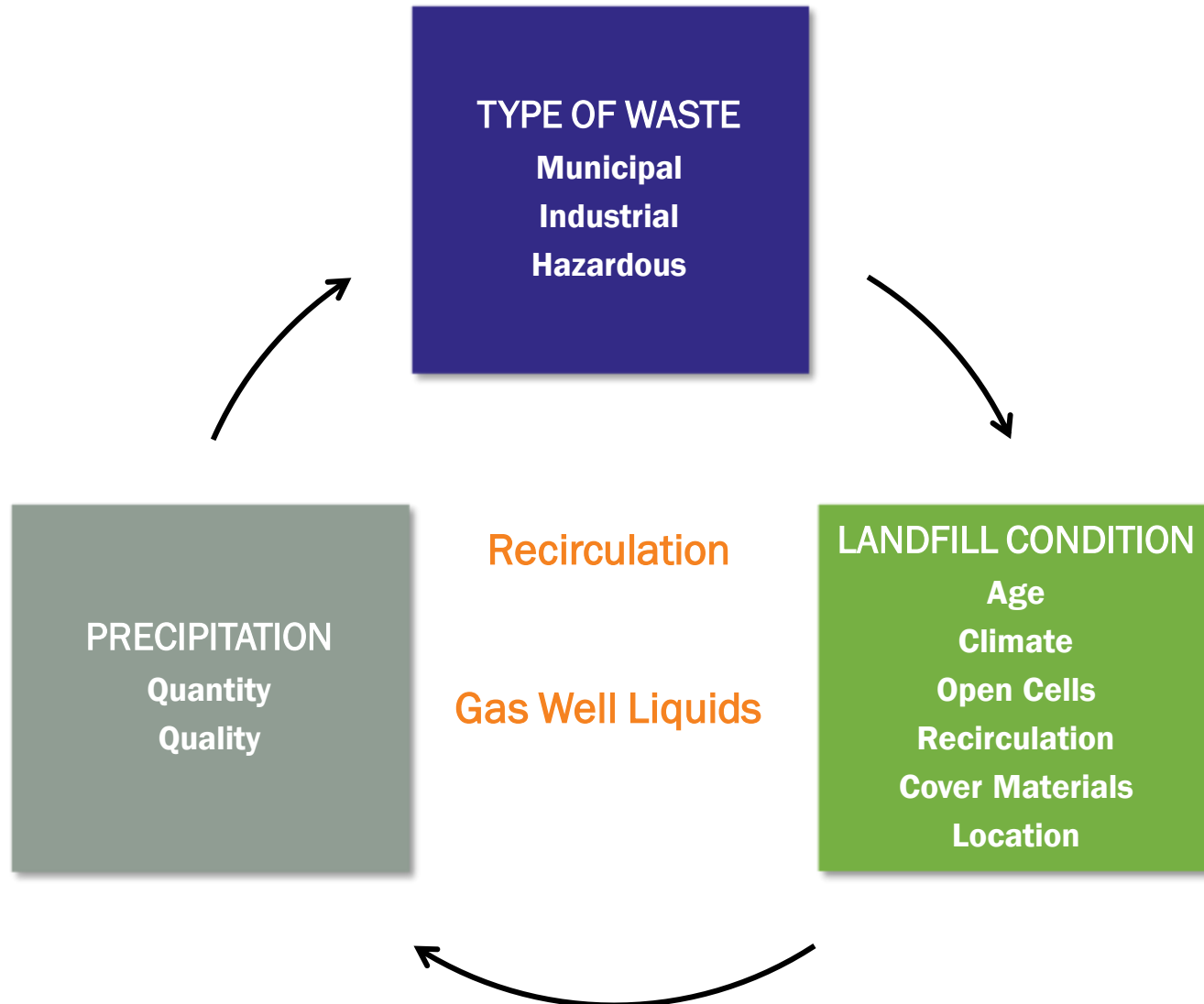
# Leachate Generation

- Rainfall (climate)
- Infiltration (cover)
- Moisture content (waste)
- Additional liquids (recirculation)



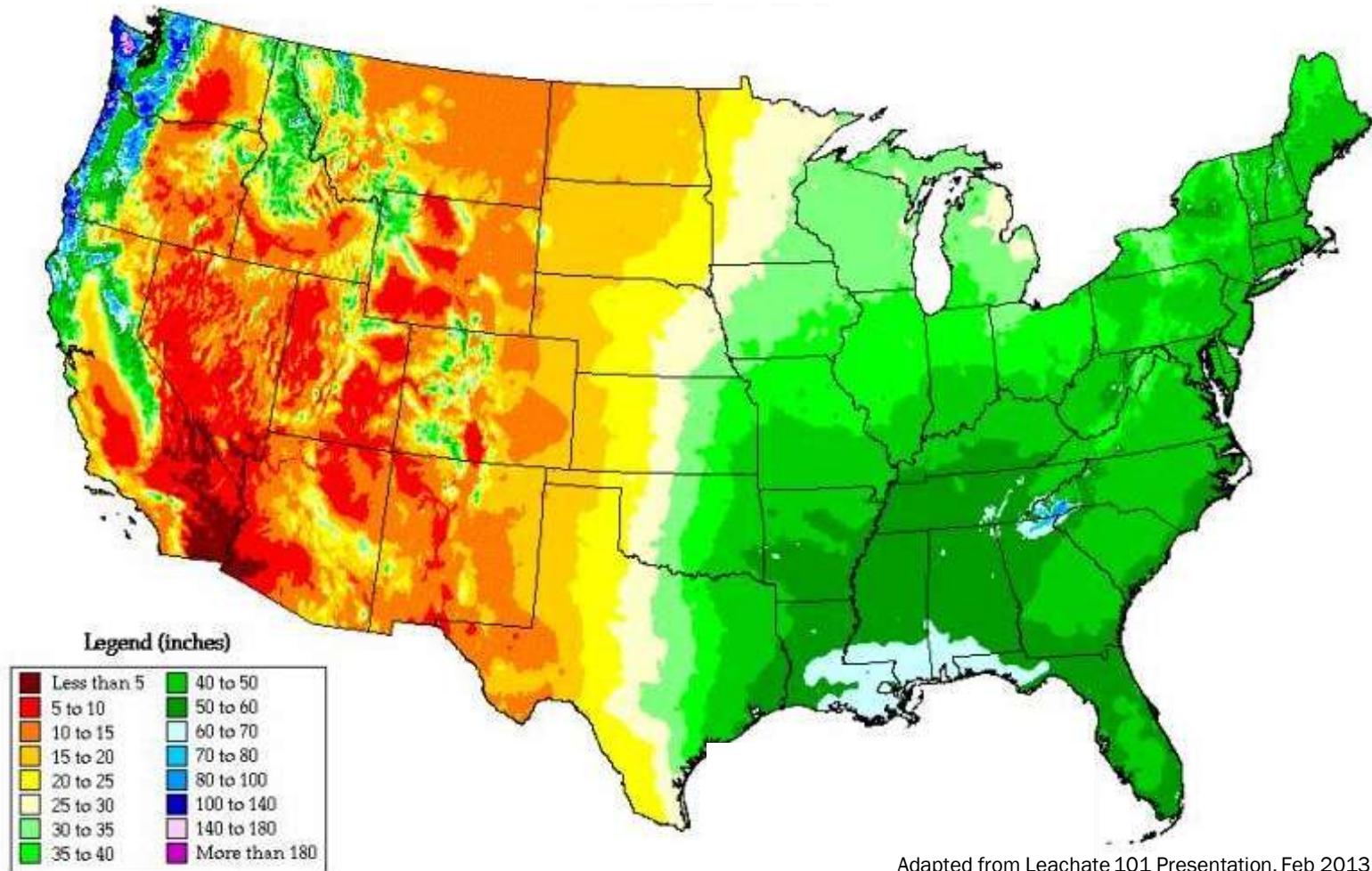
Adapted from Leachate 101 Presentation, Feb 2013

# Factors Affecting Leachate Composition



# Impacts of Climate Change on Leachate

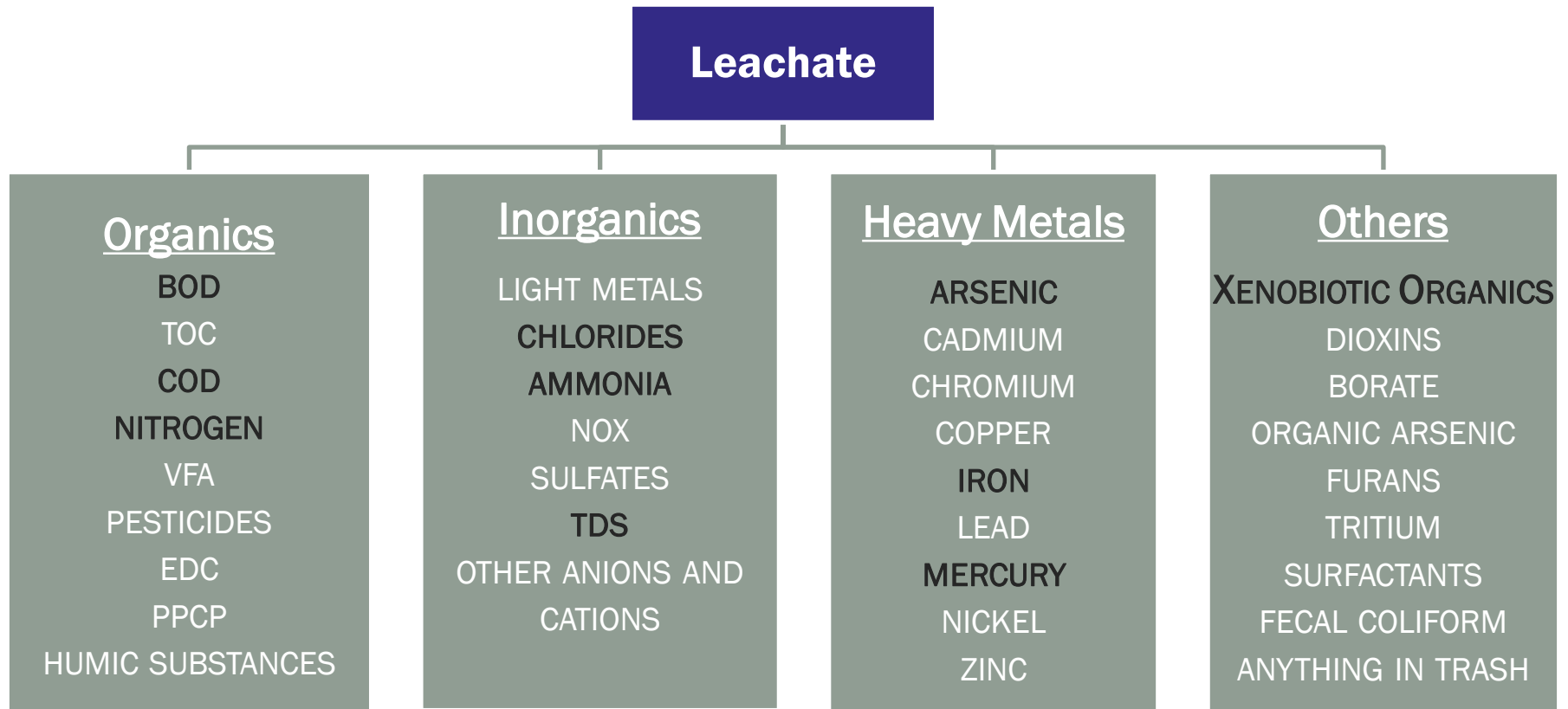
## Average Annual Precipitation in the US



Period: 1961-1990

Adapted from Leachate 101 Presentation, Feb 2013

# Leachate Composition





# MSW Leachate Composition vs. Landfill Age

Leachate Constituent	Concentration (mg/L)			
	Transition Phase 0 – 5 Yrs	Acid - Formation Phase 5 – 10 Yrs	Methane - Formation Phase 10 – 20 Yrs	Final Maturation Phase > 20 Yrs
BOD	100 – 11,000	1,000 – 57,000	100 – 3,500	4 – 120
COD	500 – 22,000	1,500 – 71,000	150 – 10,000	30 – 900
CBOD/COD Biodegradability	0.23 – 0.87 Increasing	0.4 – 0.8 High	0.17 – 0.64 Decreasing	0.02 – 0.13 Low
TOC	100 – 3,000	500 – 28,000	50 – 2,200	70 – 260
Ammonia	0 – 190	30 – 3,000	100 - 500	100 – 500
NO <sub>3</sub> - N	0 – 500	0 – 20	0 – 1.5	0 – 0.6
TDS	2,500 – 14,000	4,000 – 55,000	1,100 – 6,400	1,460 – 4,640

# MSW Leachate Composition vs. Landfill Age

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<b>Ammonia</b>	<b>0 – 190</b>	<b>30 – 3,000</b>	<b>100 - 500</b>	<b>100 – 500</b>
NO <sub>3</sub> - N	0 – 500	0 – 20	0 – 1.5	0 – 0.6
TDS	2,500 – 14,000	4,000 – 55,000	1,100 – 6,400	1,460 – 4,640

# Leachate Minimization and Management

- Leachate management system
  - Drainage layers (gravel, sand, drainage net)
  - Collection piping
- Stormwater separation
  - Geosynthetic rain cover
  - Separation berms
  - Pipe connections



Adapted from Leachate 101 Presentation, Feb 2013

# Leachate Storage Systems

## Above ground

- Steel tanks
  - Bolted, welded, glass lined, stainless, epoxy coated, lined
- Plastics
  - Tanks, impoundments

## Storage lagoons and ponds

- Geosynthetic, concrete



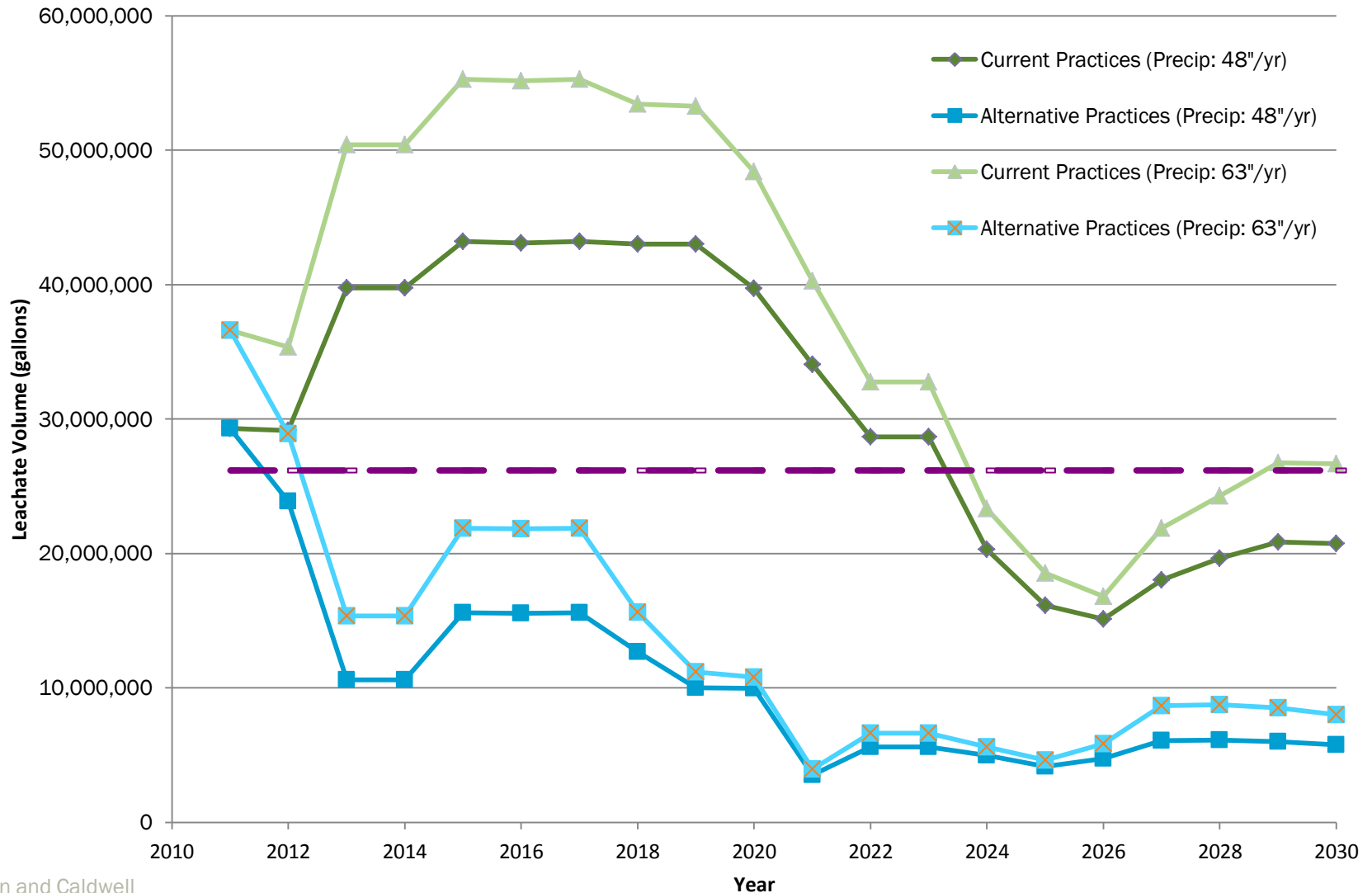


# Leachate 201



# Considerations for Disposal

# Minimization Example: Annual Projected Leachate Volume Generation



# Leachate Disposal Options

## LEACHATE COLLECTION/TREATMENT

Surface  
Water

POTW

Private  
Facility

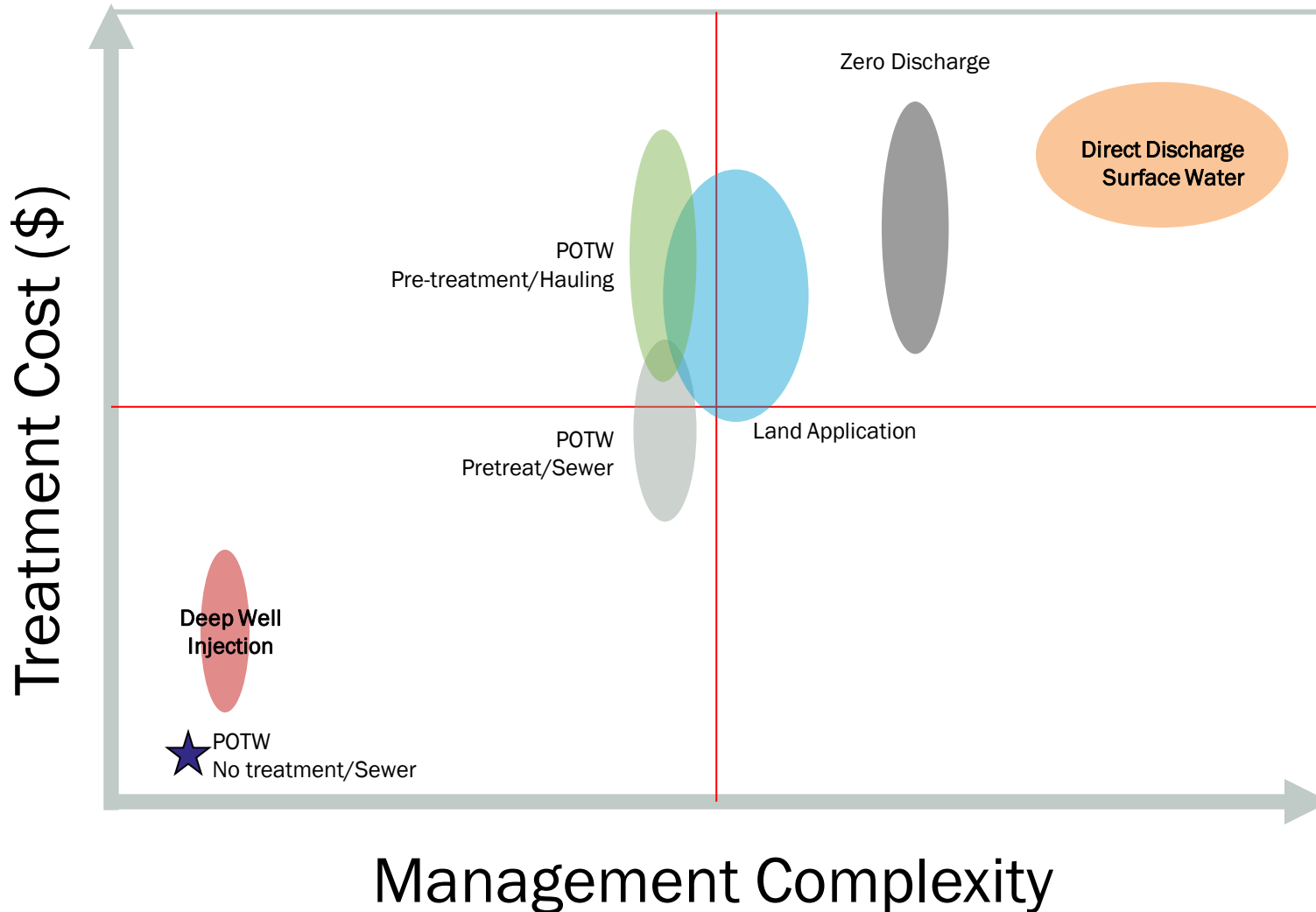
Land  
Application

Deep Well  
Injection

Zero  
Discharge



# Comparative Treatment Cost



# Selection Criteria and Key Considerations

- Leachate quality/quantity
- Land availability
- Disposal route
- Discharge limits
- Climate
- LFG availability
- Site operations capabilities
- Site preferences
- Landfill life
- Air emissions
- POTW Capacity
- POTW Processes
- Energy Costs
- Residual disposal
- Site preferences
- Minimization potential
- Etc.

## Basis for Limits

# Direct Discharge to Surface Water

## TBEL's

- Best available technology
- Established based on best professional judgment
- Federal ELGs (40 CFR Part 403)

## TMDL

- Impaired water bodies where water quality standards are not expected to be met after implementation of technology-based effluent limitations on point sources

## WQBEL

- Established when TBEL's are not stringent enough to meet State WQS
- Based on designated water body use
- Mass balance (does not apply for some pollutants)
- Mixing zone rules and limitations

## WET

- Acute toxicity limit
- Chronic toxicity limit

# Basis for Limits

## Indirect Discharge to POTWs

### Industrial Pretreatment Program

- Local discharge limits issued by local municipality or sewer agency
  - Same limit apply to all industrial users
  - Specific limits for each industrial user
- Categorical Pretreatment Standards (Federal) specific to defined categories of industries, 40 CFR 405 – 499
  - Treatment technology based limits
- Surcharges for compatible pollutants

# Comparison of Effluent Limitations

Parameter	Unit	Monthly Daily Concentrations		
		Typical POTW Pretreatment <sup>1</sup> Average	Average	Maximum
BOD <sub>5</sub>	mg/L	200 - 500	37	37
TSS	mg/L	100 - 1,000	27	27
Ammonia	mg/L	25 - 300	4.9	4.9
Zinc	mg/L	Site specific	0.11	0.11
Alpha Terpineol	mg/L	Site specific	0.016	0.016
Benzoic Acid	mg/L	Site specific	0.071	0.071
p-Cresol	mg/L	Site specific	0.014	0.014
Phenol	mg/L	Site specific	0.015	0.015
pH	std. units		6.0 - 9.0	

## Notes

1. General range of POTW is compiled based on project experience
2. Table 2-2 Non-Hazardous Landfill Subcategory , EPA-821-R-99-019
3. Site specific discharge permits will likely require additional parameter monitoring and/or impose additional parameter limitations

# Other Regulatory Considerations

- Air emission
  - Storage
  - Treatment/Pretreatment
  - Zero discharge
  - Land application?
- Groundwater protection/quality
  - Land application
  - Deep well injection
- Residuals management
  - Treatment/Pretreatment
  - Zero discharge
  - Land application?
  - Deep well injection?
- OSHA-Virtually all

# Leachate Disposal Costs Example

Landfill	Management	Costs	Notes
A	<b>Option 1:</b> Raw leachate discharged to a POTW -X through sewer connection	\$0.02/gal (1) typical range: \$0.02 to \$0.05	Annual savings > \$200,000/yr Compared to Option 2
	<b>Option 2:</b> Hauling raw leachate to a POTW-Y	\$0.055/gal	
B	Direct discharge to surface water	\$0.05/gal (2) typical range: \$0.02 - \$0.05 \$0.02 (less stringent limits) \$0.05 (very stringent limits)	Membrane Bioreactor (MBR) Technology

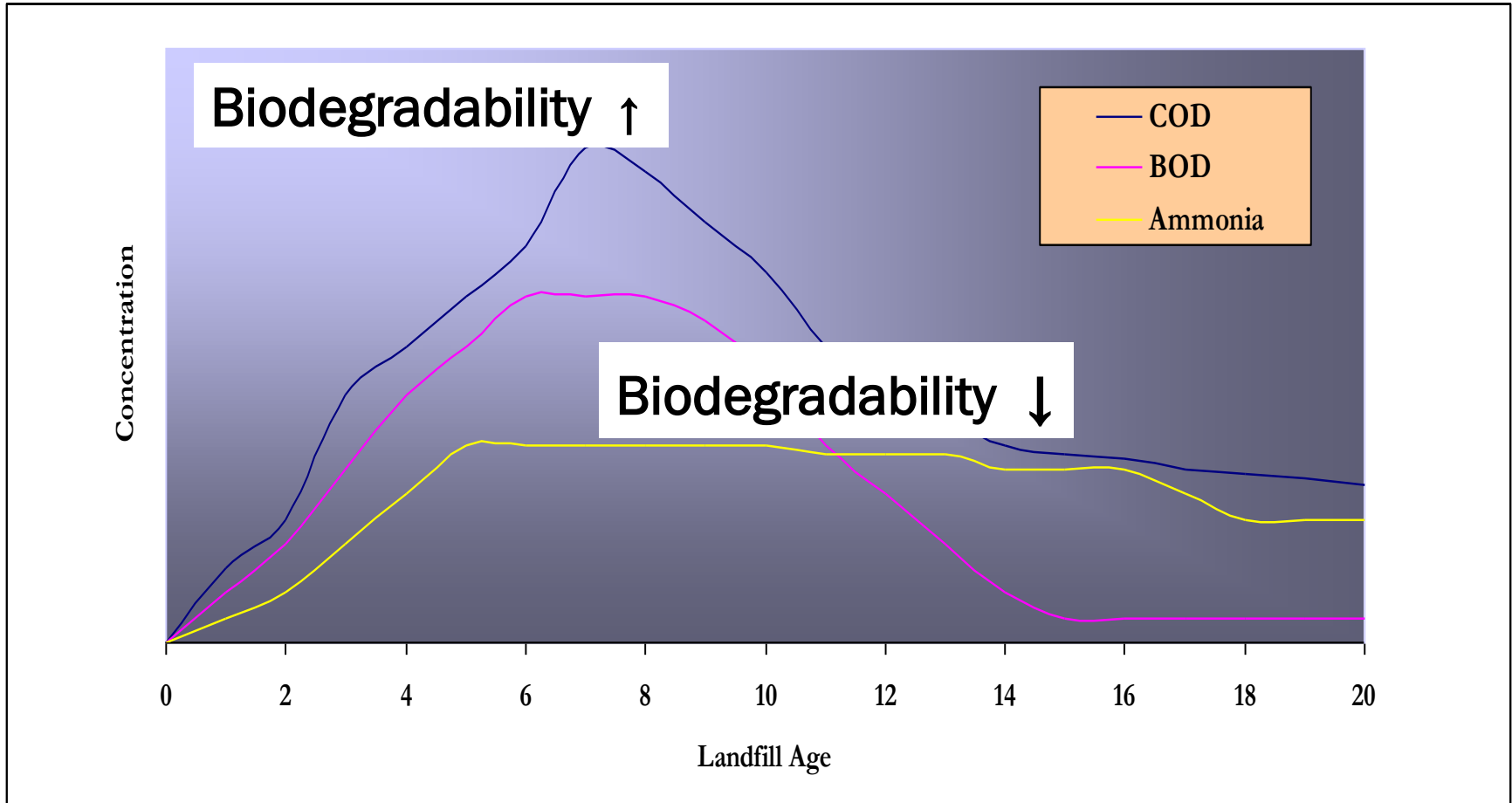
- Notes
1. Includes surcharges for NH<sub>3</sub>-N, TSS, and BOD on a mass basis (\$/lb); analytical, sampling and sewer connection costs.
  2. Includes amortized capital costs for equipment purchase and installation, O&M costs over a 20-year period.



# Offsite Disposal - Issues for POTWs



# Leachate Characteristics vs. Landfill Age



# MSW Leachate vs. Domestic Wastewater Composition

Parameter	Unit	Domestic Wastewater <sup>1</sup>		Landfill Leachate		
		Weak/Medium	Strong	MSW	Ash-fill <sup>3</sup>	C&D <sup>4</sup>
BOD	mg/L	110 - 190	350	500 - 3,300	4 - 100	
COD	mg/L	250 - 430	800	1,800 - 4,350	500 - 2,000	150 - 700
TOC	mg/L	80 - 140	260	-	10 - 80	20 - 625
Ammonia	mg/L	12 - 25	45	150 - 2,250	25 - 90	
NO <sub>2</sub> /NO <sub>3</sub>	mg/L	0	0	0		
Total P	mg/L	4 - 7	12	3 - 10		
TSS	mg/L	120 - 210	400	50 - 150	15 - 60	

## Notes

1. Adapted from Table 3-15 from Metcalf & Eddy, 4<sup>th</sup> Edition
2. Observations from onsite storage tanks
3. Observations from with segregated leachate streams
4. Townsend et al. 2000.

# MSW Leachate vs. Domestic Wastewater

**MSW Leachate is 10 – 70 times the strength of domestic sewage and reacts differently in treatment**

Parameter	Unit	Domestic Wastewater <sup>1</sup>		Landfill Leachate		
		Weak/Medium	Strong	MSW <sup>2</sup>	Ash-fill <sup>3</sup>	C&D <sup>4</sup>
BOD	mg/L	110 – 190	350	500 – 3,300	4 – 100	
COD	mg/L	250 – 430	800	1,800 – 4,350	500 – 2,100	150 - 700
TOC	mg/L	80 – 140	260	-	10 – 80	20 - 625
Ammonia	mg/L	12 – 25	45	150 – 2,250	25 – 100	
NO <sub>2</sub> /NO <sub>3</sub>	mg/L	0	0	0		
Total P	mg/L	4 – 7	12	3 - 10		
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		Weak/Medium	Strong	MSW	Ash-fill <sup>3</sup>	C&D <sup>4</sup>
pH	mg/L	-	-	6.8 – 7.5		6.0 – 8.0
TDS	mg/L	270 – 500	860	5,000 – 20,000	25,000 – 50,000	1,000 – 6,000
Alkalinity as CaCO <sub>3</sub>	mg/L	50 - 100	200	850 – 8,000	50 - 100	-
Hardness as CaCO <sub>3</sub>	mg/L			-		-
Chloride	mg/L	30 – 50	100	750 – 1,200	15,000 – 25,000	10 – 6,000
Sulfate	mg/L	20 – 30	50	150 - 500	600 – 1,000	30 – 2,100
VOC/SVOC	mg/L					

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<b>TDS</b>	<b>mg/L</b>	270 – 500	860	5,000 – 20,000	25,000 – 50,000	1,000 – 6,000
Alkalinity as CaCO <sub>3</sub>	mg/L	50 - 100	200	850 – 8,000	50 - 100	-
Hardness as CaCO <sub>3</sub>	mg/L			-		-
<b>Chloride</b>	<b>mg/L</b>	30 – 50	100	750 – 1,200	15,000 – 25,000	10 – 6,000
<b>Sulfate</b>	<b>mg/L</b>	20 – 30	50	150 - 500	600 – 1,000	30 – 2,100
VOC/SVOC	mg/L			BRL – 0.5		

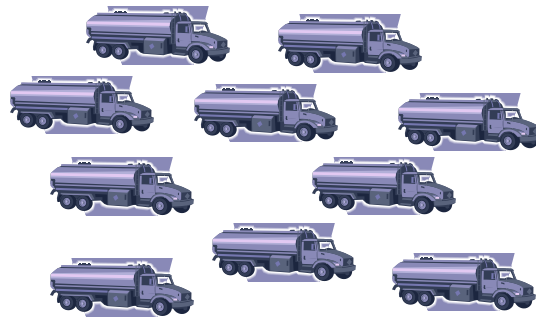
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4. Townsend et al. 2000.

# MSW Leachate vs. Gas Well Condensate

Parameter	Unit	Landfill Leachate	Condensate
		Typical	Observed
BOD	mg/L	500 – 3,300	1,000 – 10,000 +
COD	mg/L	1,800 – 4,350	3,000 – 20,000+
Ammonia	mg/L	150 – 2,250	500 – 10,000
NO <sub>2</sub> /NO <sub>3</sub>	mg/L	0	-
VOC/SVOC	mg/L	Varied	5x – 10x, possibly free product
TDS	mg/L	500 – 5,000	3,000 – 50,000+

# Comparative Waste Loadings (Rule of Thumb)



**Domestic WW**  
**1 Equivalent**

**MSW Leachate**  
**10 Equivalents**

**Condensate**  
**30 Equivalents**

# Potential Impacts to POTWs

- Ammonia removal inhibition
- Biological treatment upset
- Metals (e.g., arsenic)
- Color
- UV transmittance (POTW issue)
- TDS/Chlorides (e.g. deflocculation, pass through into effluent)
- Refractory dissolved organic nitrogen (rDON)
- Non-degradable COD
- Odors
- Foaming
- Sulfate (sewer odor)





# Most Common Problematic Parameters

Ammonia

COD/BOD

Metals

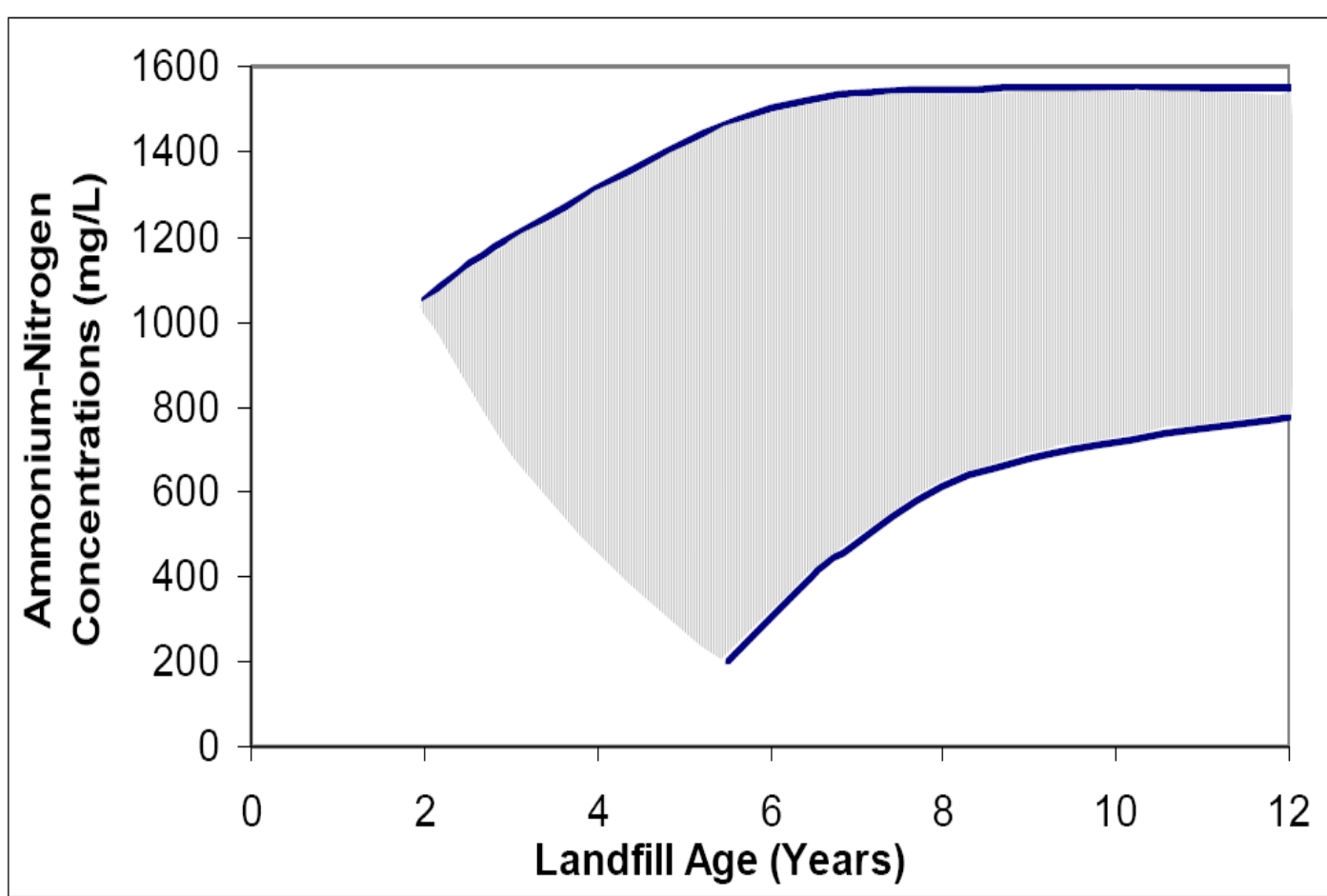
**Total nitrogen (TN) limits are becoming more common in discharge permits (POTW and Discharge – NPDES) requiring advanced treatment**

# Why Nitrogen?

- **Toxicity** (unionized ammonia is gaseous, and toxic to fish)
- **Oxygen Depletion** (adversely affects aquatic life)
- **Eutrophication** (algal growth)
- **Reduced Chlorination Efficiency** (during disinfection, i.e. chloramines)
- **Corrosion** (ammonia)
- **Blue Baby Syndrome** (blood cannot carry oxygen to cells)
  - $\text{NO}_x$  and ammonia



# Ammonia-N vs. Landfill Age



# Aerobic Biological Treatment

- Commonly used (landfill bioreactor, constructed wetland, onsite WWTF, POTW)
- Most operators are cognizant of operational requirements



# BOD/COD and Ammonia Interaction

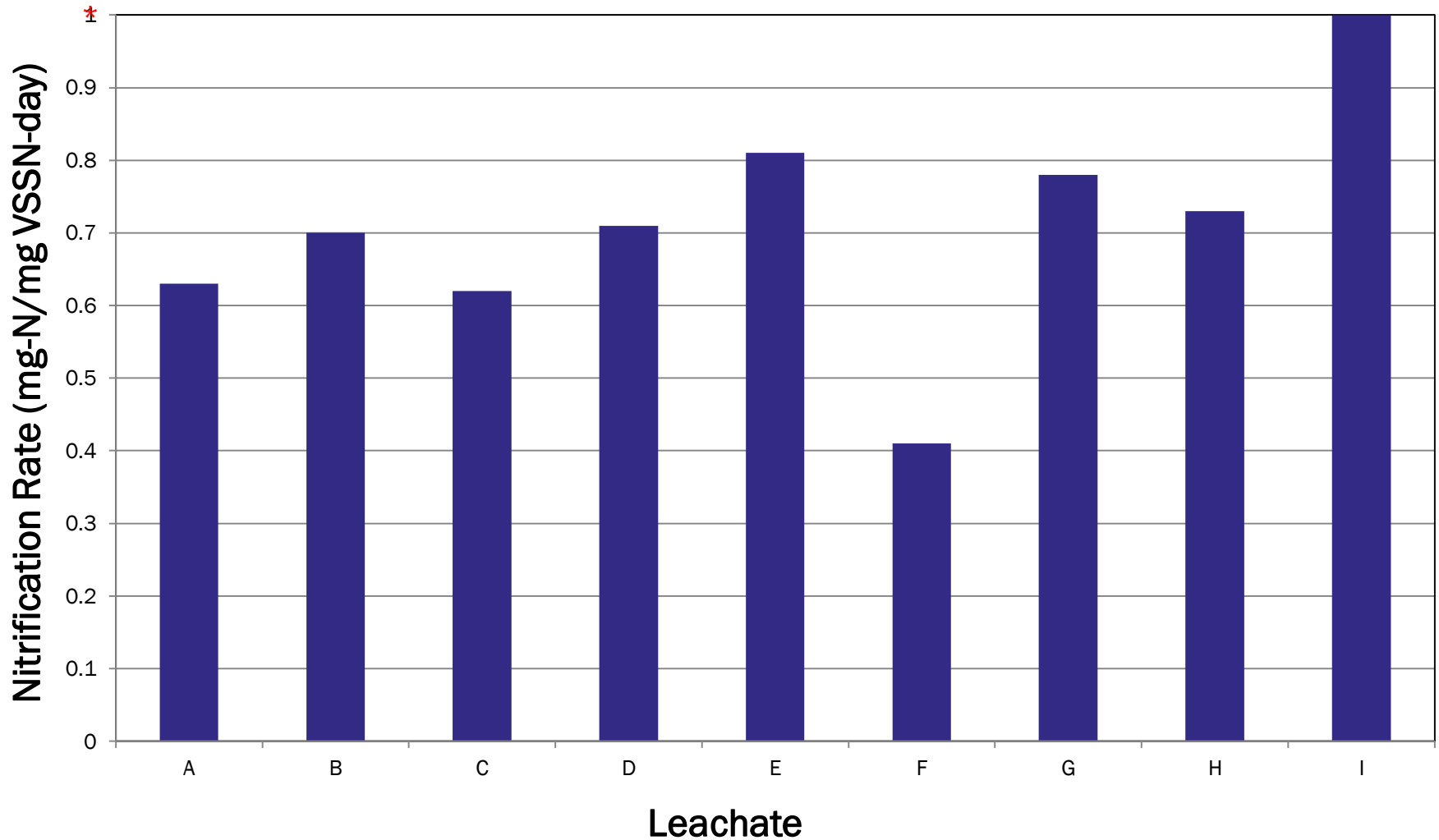
- Heterotrophs faster growing bacteria than nitrifiers
- Nitrification rates tend to drive the size of sludge age and size of basin
- Once ammonia removal accomplished, carbonaceous organic concentrations general significantly lowered
- Typically not concerned about BOD removal rates but they can be inhibited in similar fashion to nitrifiers



# Nitrification Considerations

- Nitrifiers are slow growers (define reactor size/sludge age)
- Nitrification tends to be an “all-or-none” phenomenon (on or off)
- Nitrifier floc don't settle well--need heterotrophs or BOD consuming bacteria to form a good settling floc or a robust solids/liquid separation process
- Kinetics of growth are very sensitive to:
  - Temperature (10 Deg C > range < 32 Deg C, significant decrease in rate beyond this range)
  - Alkalinity (3.7 g of CaCO<sub>3</sub> / g N removed); pH (optimal 7.5 - 8.6 s.u.)
  - Dissolved oxygen (> 2 mg/L)
  - Prone to toxicity (i.e. metals, unionized ammonia)

# Nitrogen: Range of Nitrification Rates



\*uninhibited removal rate



# Leachate Treatment Technologies & Application



# When Selecting a Technology, Consider...

## 1 Is it flexible?

Able to meet current and future stringent limits

## 2 Is it consistent and reliable?

Able to adapt to various situations

## 3 Does it offer ease of use and lowest life cycle costs?

Low on capital and O&M



# Treatment Approaches

## Physical/Chemical



## Biological



# Physical/Chemical Technologies

## Physical Treatment Examples

- Precipitation/flocculation/sedimentation
- Media filtration
- Membrane filtration
- Ion exchange/adsorption
- Air/Ammonia stripping
- Flash distillation
- RO

## Chemical Treatment Examples

- Chemical/advanced oxidation
  - Break point chlorination
  - Fenton oxidation
  - Ozone/hydrogen peroxide
  - UV based processes not applicable
- **Evaporation (volume reduction)**

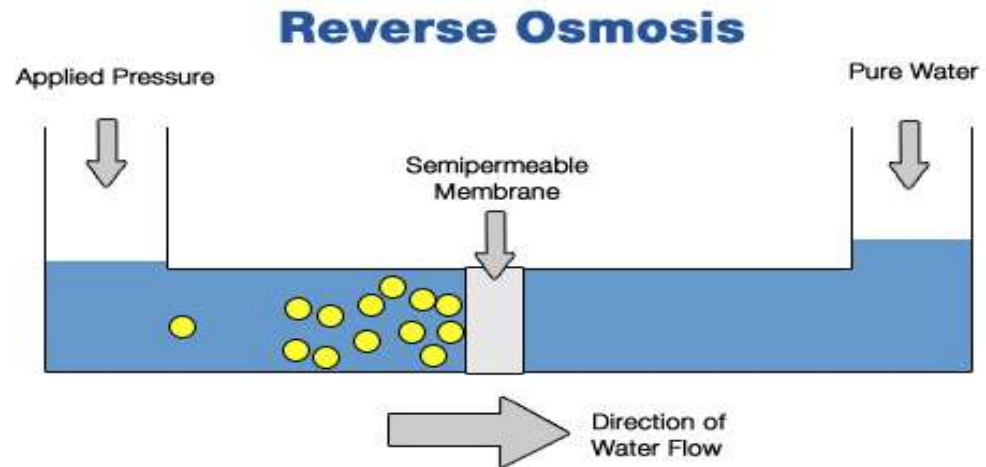


# General Observations: Non-Biological Processes

- **Non-destructive, phase transfer (liquid to solid or vapor)**
- None are generally capable of serving as a stand alone technology for direct discharge (e.g. surface water)
- Most are mechanically simple but may be operationally intensive (backwashing, media change outs, etc.)
- Leachate composition makes selective removal unlikely
- RO possible but may require upfront pre-treatment (solids and colloidal organics) and post treatment (ammonia, organics, pH, ion supplementation)
- **Residuals management can be problematic**

# Reverse Osmosis (RO)

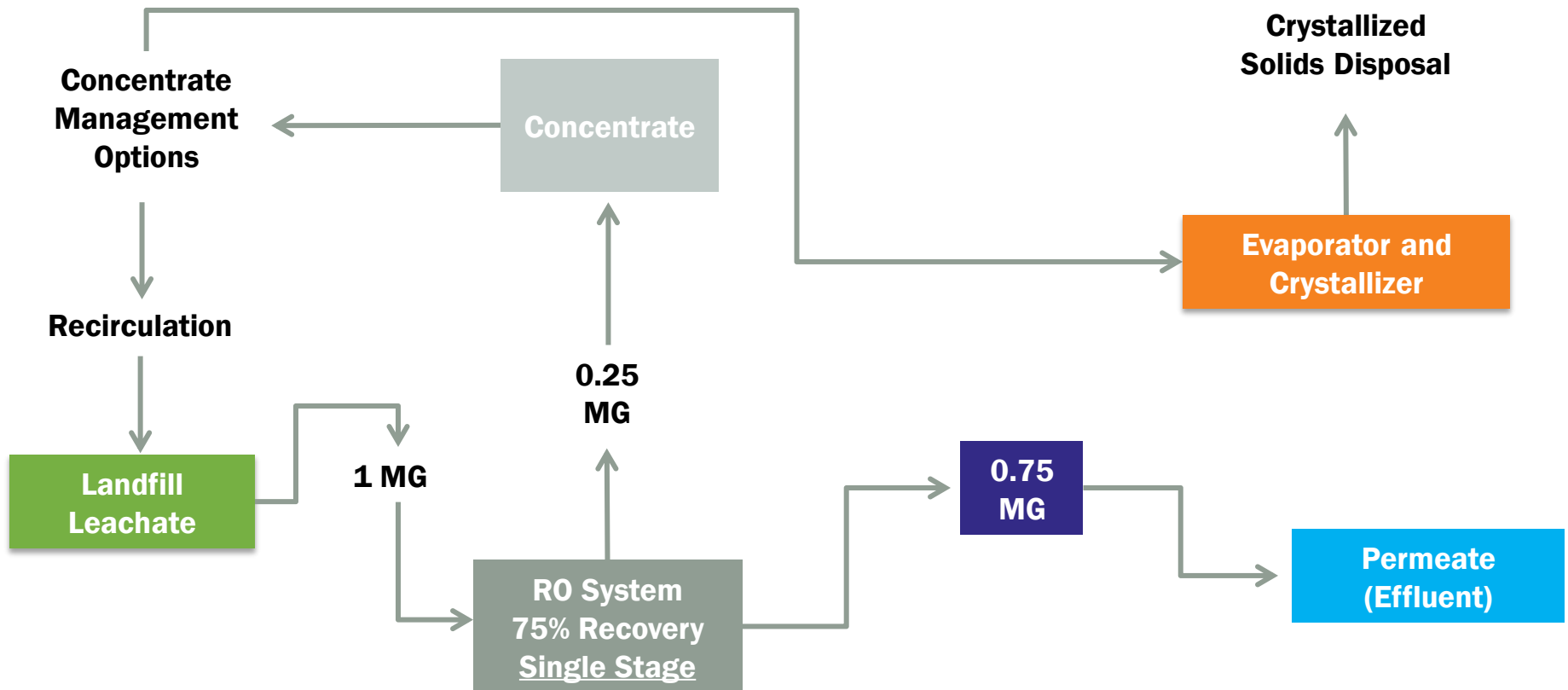
- Membrane technology
- Highest level of treatment
- Physical barrier < 0.001 micron-meter
- Performance expressed in MWC0
  - *Lower MWC0 means tighter membrane*
- Future application: TDS, color, ECOC: EDCs and PPCPs removal



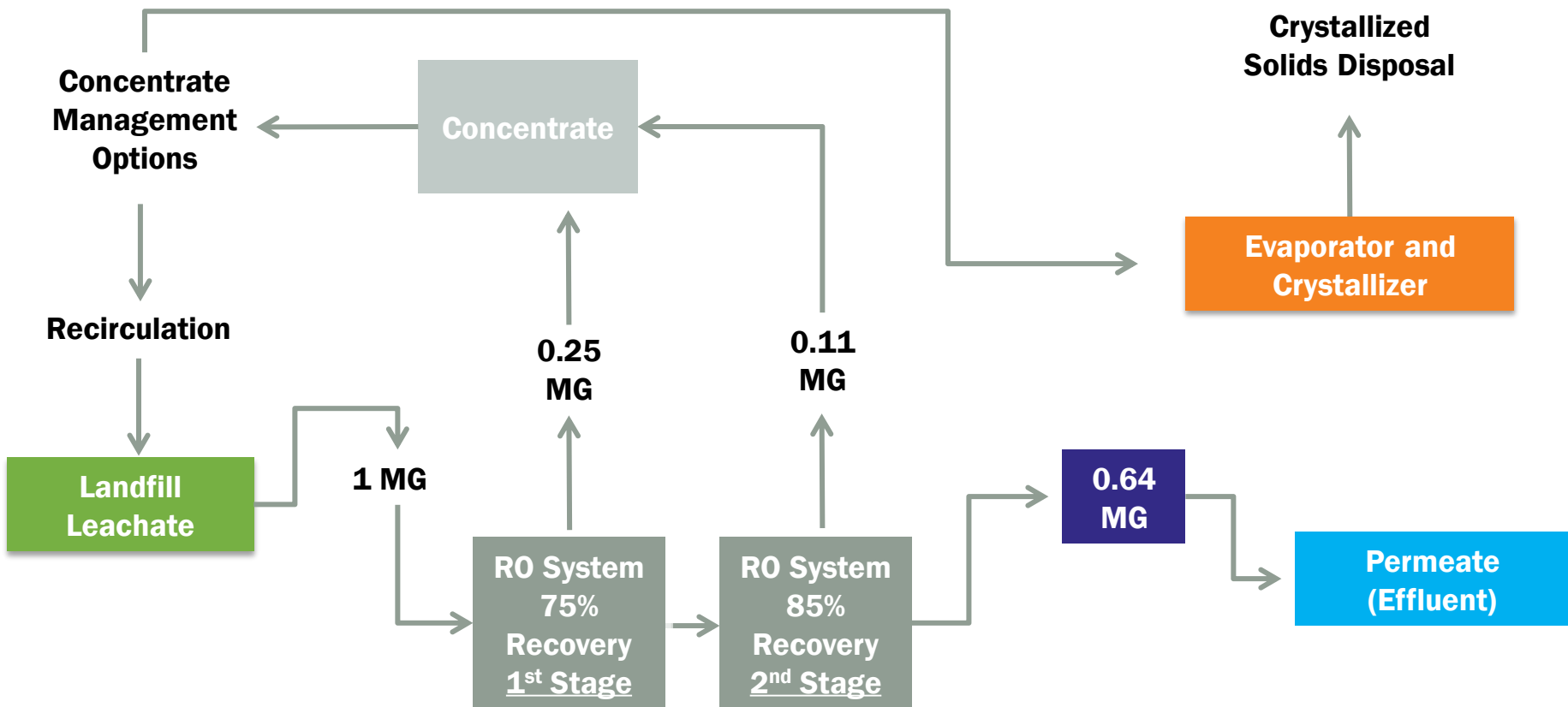
# Example RO Processes



# RO: Process Flow Single Stage Process



# RO: Process Flow Two Stage Process

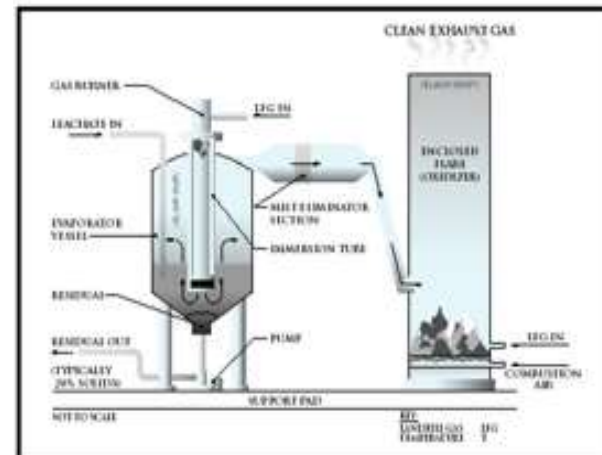


**More RO Stages will Reduce Overall System Recovery!!**  
**Multiple Stages are Required to meet Effluent NH<sub>3</sub>-N Quality**

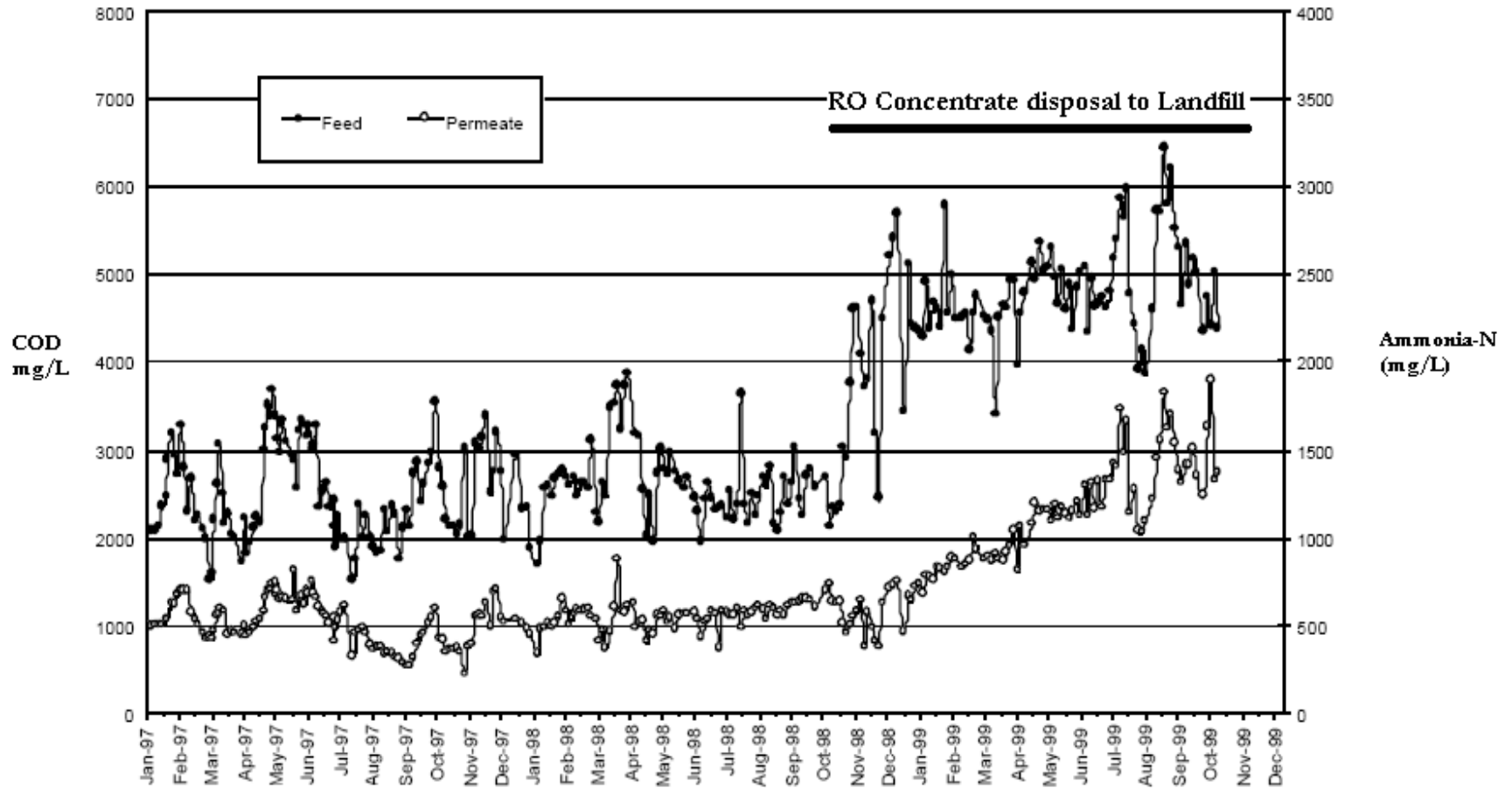


# Evaporation

- Typically 80-90% volume reduction
- Small footprint
- Flexible fuel source (waste heat, LFG, NG, LP)
- Air emission
- Residuals management



# Impacts of RO Concentrate Recirculation – COD and NH3-N



# Biological Removal: General Observations

- Constituents are removed, destroyed or transformed
- Most commonly applied treatment strategy
- Can operate as stand alone treatment systems
- Can operate over a wide variety of leachate conditions
- Leachate inhibits nitrification (factor into design)
- Operational/labor requirements vary widely
- Treatment costs tend to be lower than the physical removal strategies

# Biological Strategies

## Natural Systems

- Lagoons
- Constructed/engineered wetlands
- Phytoremediation
  - Poplar and Willow Trees
  - Vertiver grass
  - Shrubs



# Biological Strategies

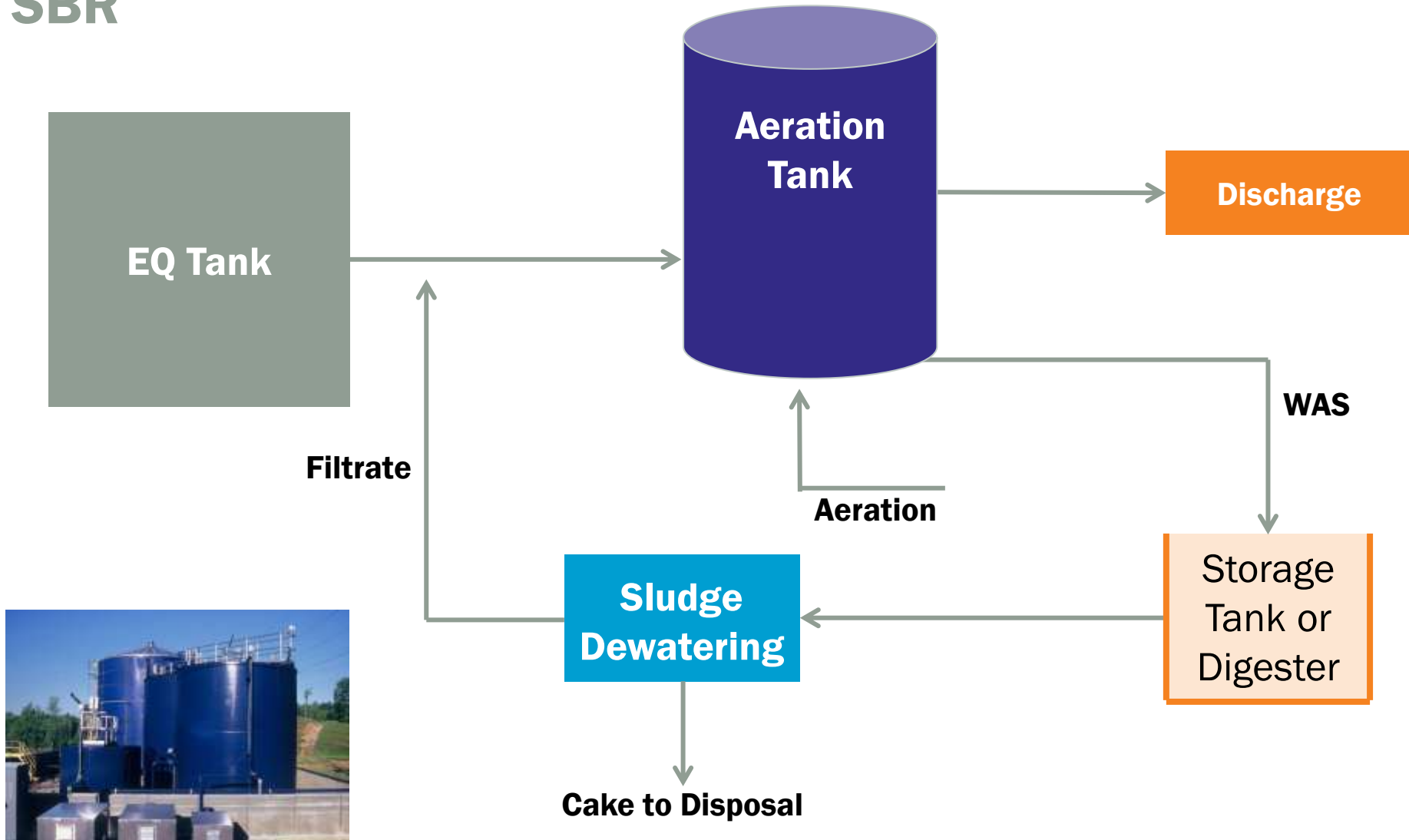
## Tank Based Biological

- Sequencing batch reactors (SBR)
- Membrane bioreactors (MBR)
- Conventional activated sludge (AS)
- Powdered activated carbon treatment (PACT)
- Moving bed biofilm/biological reactor (MBBR)
- Integrated fixed-film activated sludge (IFAS)
- Fixed film

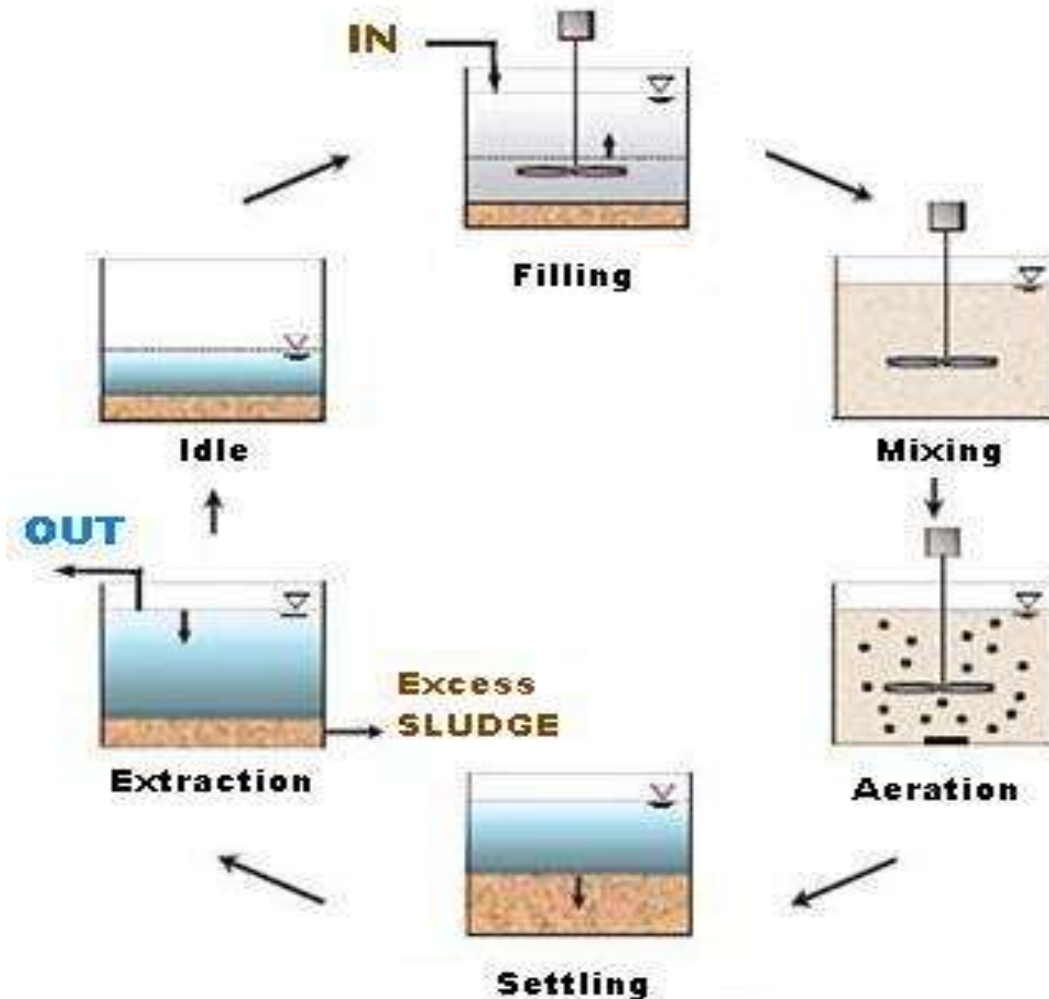


# Sample Treatment System Configurations

## SBR



# SBR Process Single Tank Operation Steps



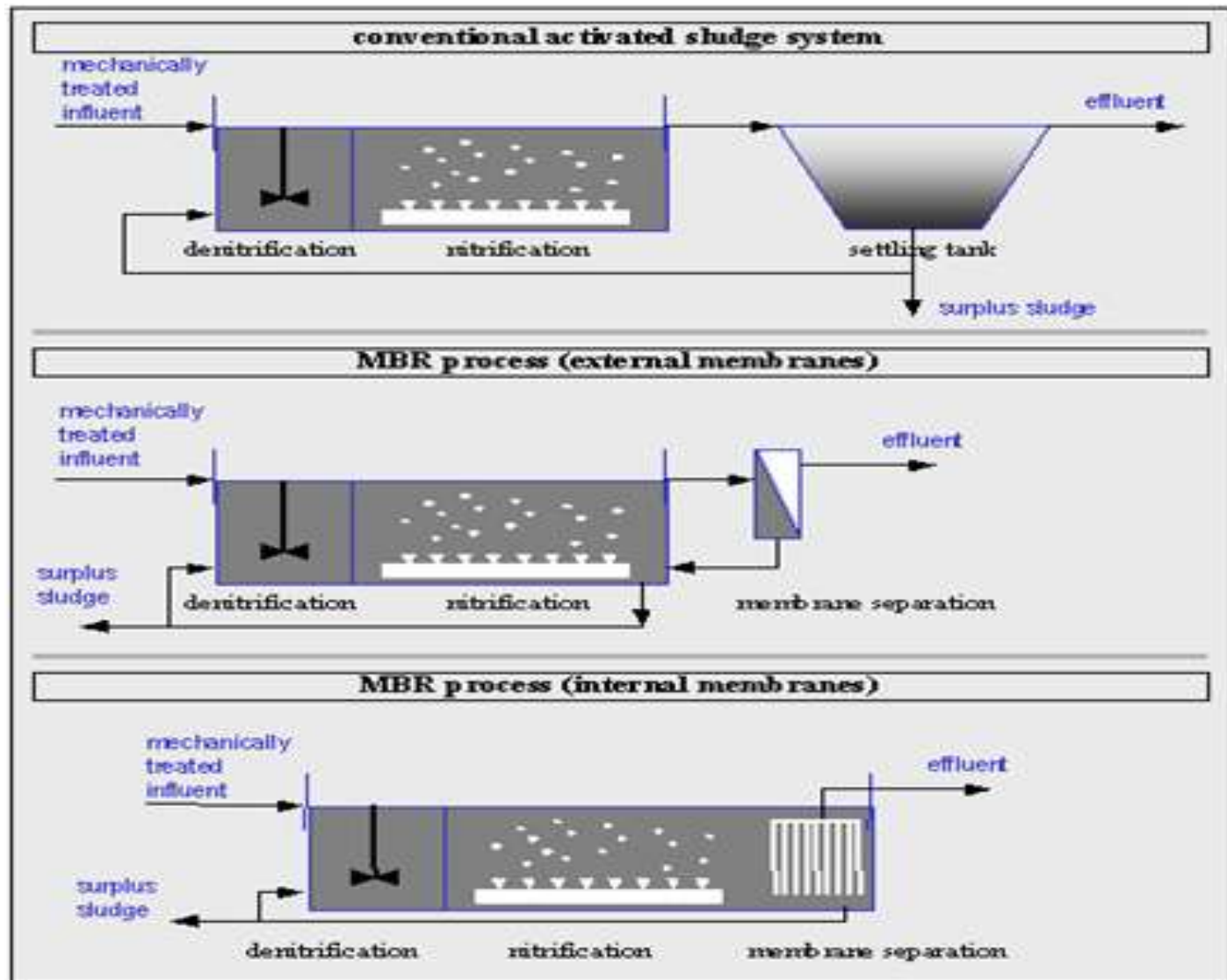
# Membrane BioReactor Treatment

## MBR: Activated Sludge Followed by Ultrafiltration

- Physical Barrier
  - 0.01 – 0.05  $\mu\text{m}$  nominal pore size (RO is 2 orders of magnitude smaller than UF)
  - Current disc filter nominal pore size is 10  $\mu\text{m}$  (2-3 orders of magnitude larger than UF)
- Replaces conventional clarifier thus avoiding sludge settling and contaminant carryover issues
- Eliminates need for additional filtration
- Uses automated cleaning and back-pulsing for membrane maintenance

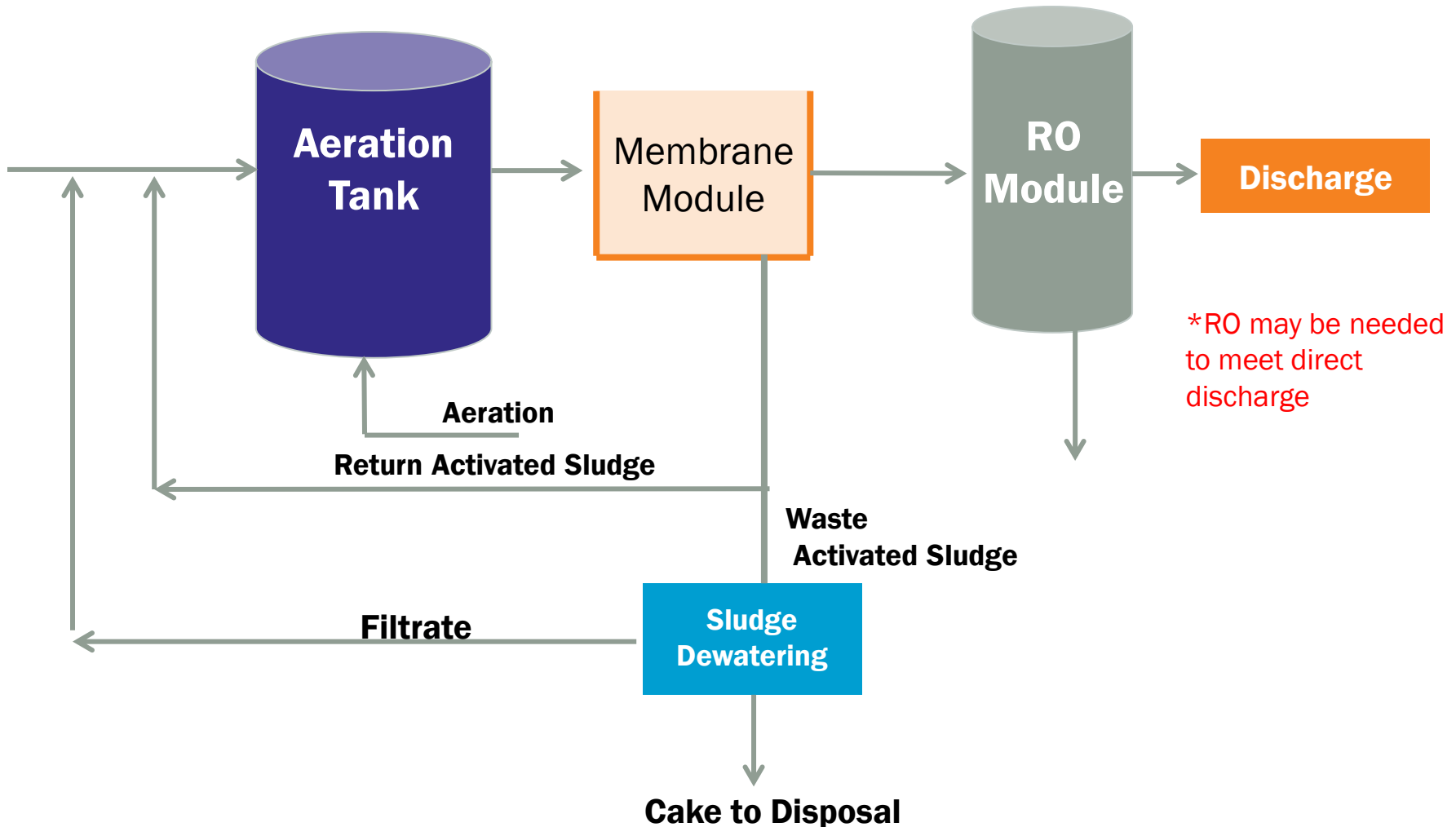


# MBR Process Comparison

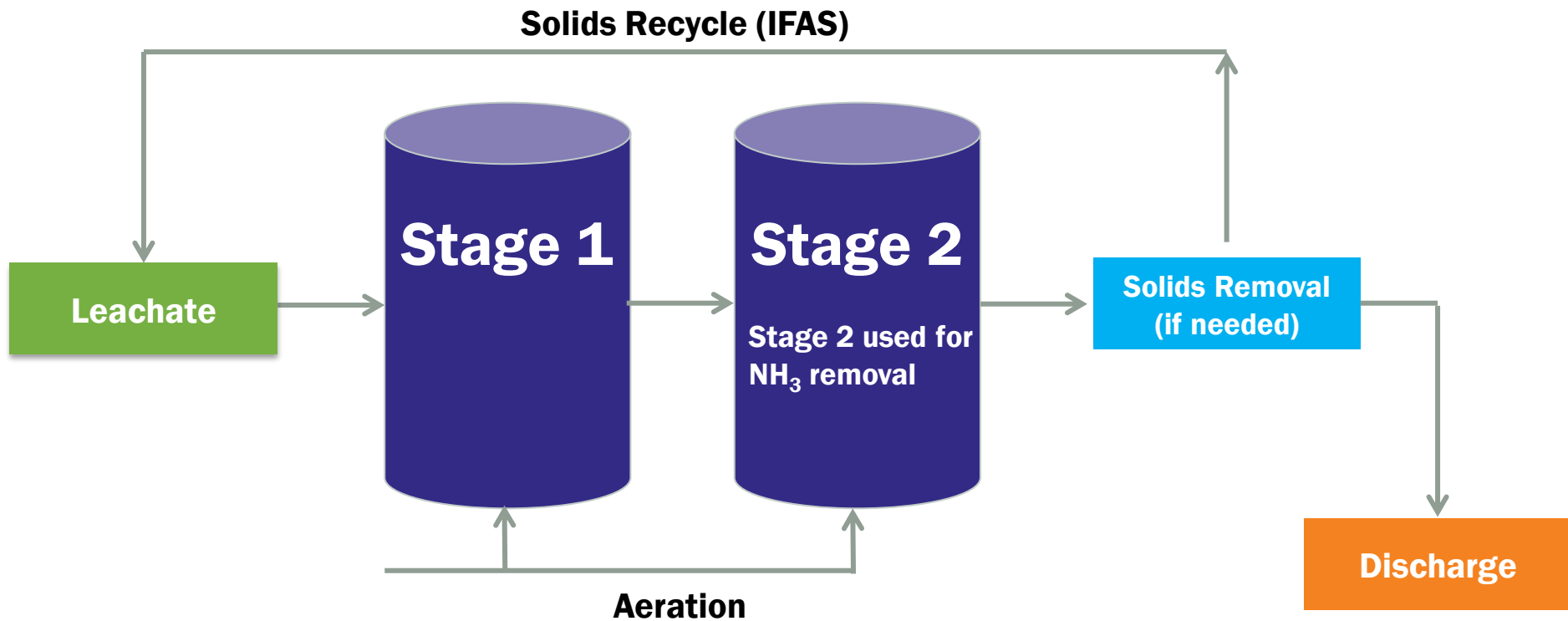


# Sample Treatment System Configurations

## MBR/MBR-RO



# MBBR/IFAS

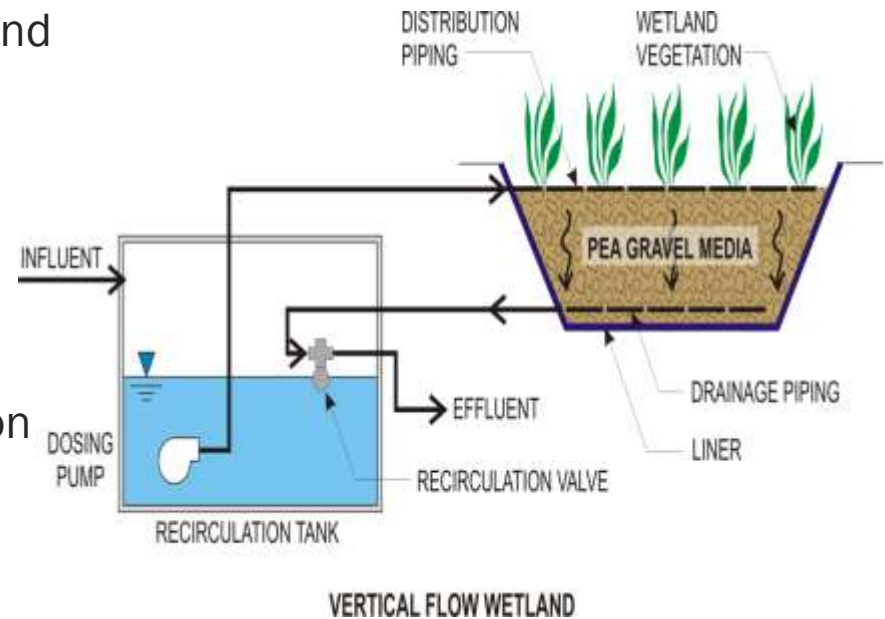


# Moving Bed Bioreactor (MBBR)



# Constructed Wetlands

- Plants and bacteria use ammonia-N as a nitrogen source
  - Plants: hyacinth
- Nitrification
- Surface flow (SF), subsurface flow (SSF), and hybrid wetlands
- SSF
  - Horizontal and vertical flow
  - Higher efficiency than SF
  - More temperature resistance than SF (freezing)
- Fill Material
  - Plants, sand, gravel, wood chips (carbon source)
- SSF = horizontal flow wetlands
  - Denitrification (wood chips)
- SSF = vertical flow wetlands
  - Ammonia removal
  - Facilitates oxygen transfer from the atmosphere



# Issues on the Horizon

## Near Term

- Color
- UV transmittance (POTW)
- Nutrients
- Refractory Dissolved Organic Nitrogen
- Total Dissolved Solids/  
chlorides



Brown and Caldwell



## Longer Term

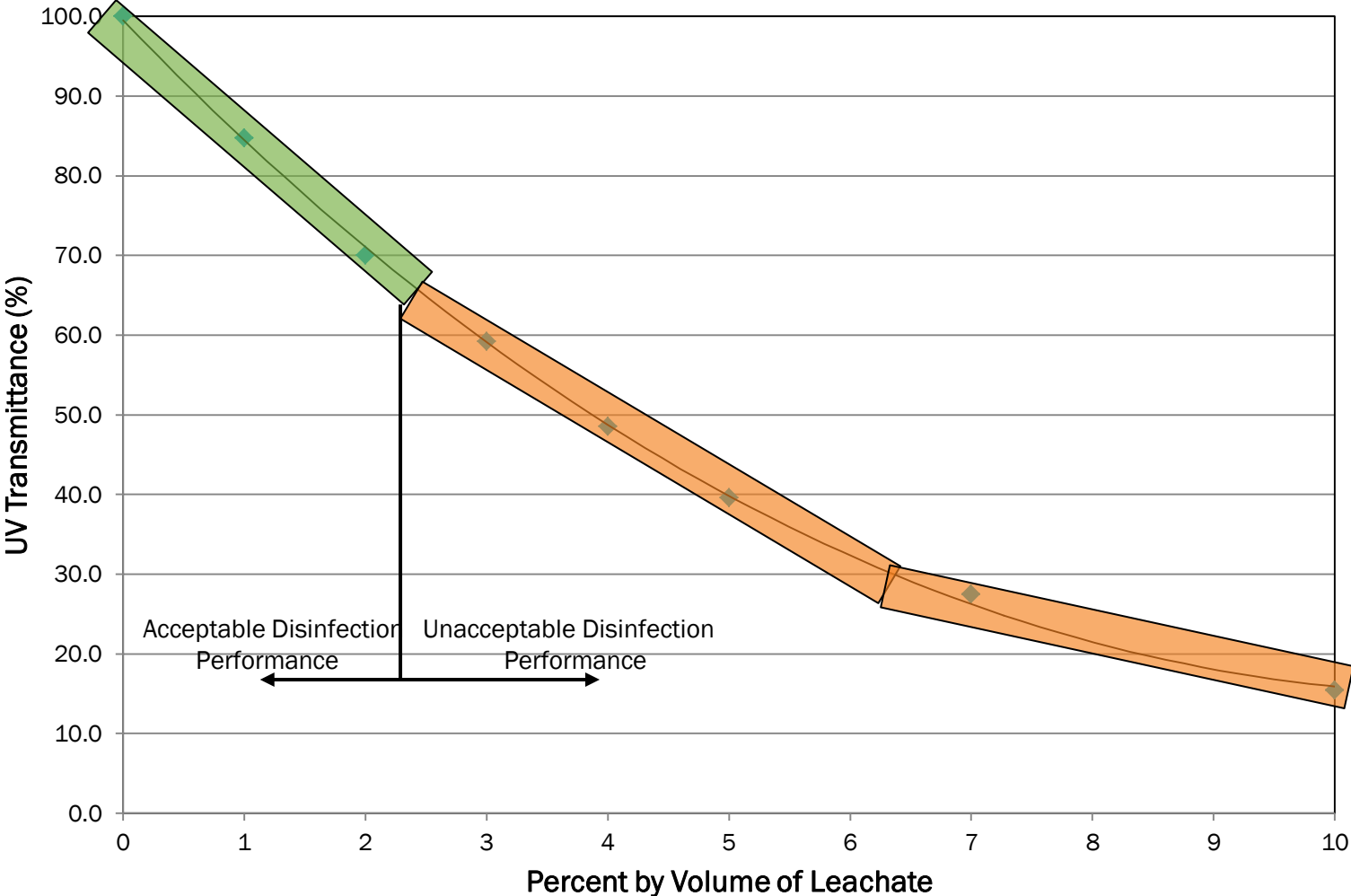
- Emerging contaminants
  - Boron, PFCs, future unknowns
- Pharmaceutical and Personal Care Products
- Nano-particles



# Emerging Contaminants: EDC & PPCP

- A recent study by the MaineDEP showed that PPCPs were present in landfill leachate
- Raw leachate samples from three MSW landfills were analyzed for 135 individual pharmaceutical and health care products
- The analytical results showed that the samples contained approximately **40 pharmaceutical compounds**
- Pharmaceuticals are discarded in household waste and appear in landfill leachate
- Regulatory agencies may try to regulate the release of pharmaceuticals to receiving streams from POTWs because of the toxic impacts to aquatic life (e.g. sex changes in fish)
- Drive to educate public to eliminate sewerage of unused pharmaceuticals. Anticipate higher volumes of pharmaceuticals being directed to landfills

# UVT: Effect of Leachate on UVT at POTW





# UVT and Color: No Clear Correlation

Matrix Treatment	True Color (PCU)	UVT (%)
Raw Leachate	1950	0
Perozone (2,000 ppm) with 12 Minute Contact Time	105	0.2
Chlorination (1,000 ppm) with 1 Hour Contact Time	100	0.1
Chlorination (1,000 ppm) with 18 Hour Contact Time	50	0.1

# Color/UV Transmittance

## Landfill A

- Raw leachate color = 4,000 – 4,500 PCU
- Current LTP limit = 1,500 PCU was reduced to 100 PCU for future new LTP
- BAT: Emphasis on costs and other non environmental factors
- Waiver request to 2,000 PCU (in progress)

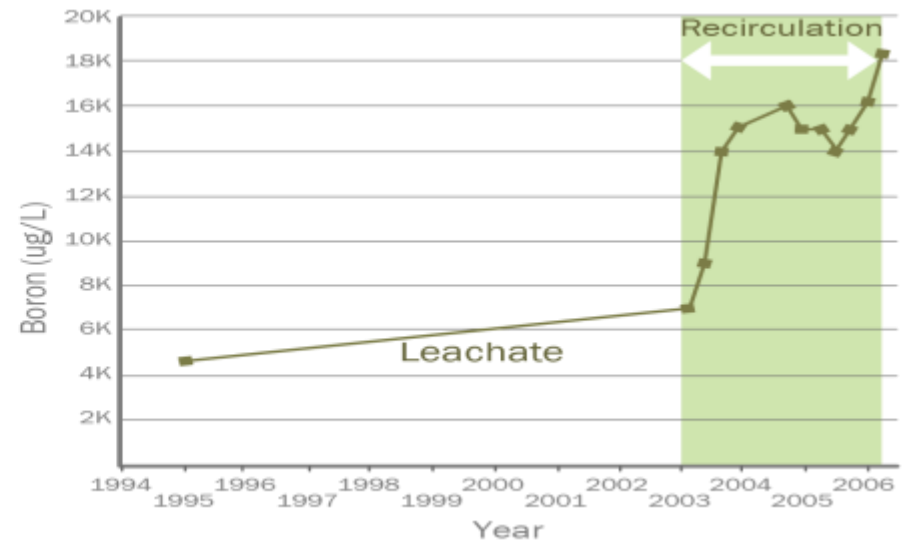
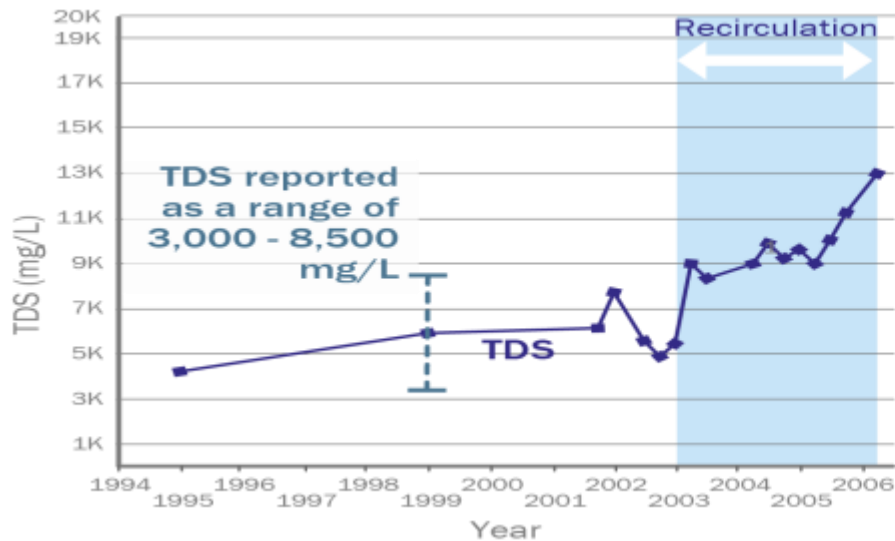
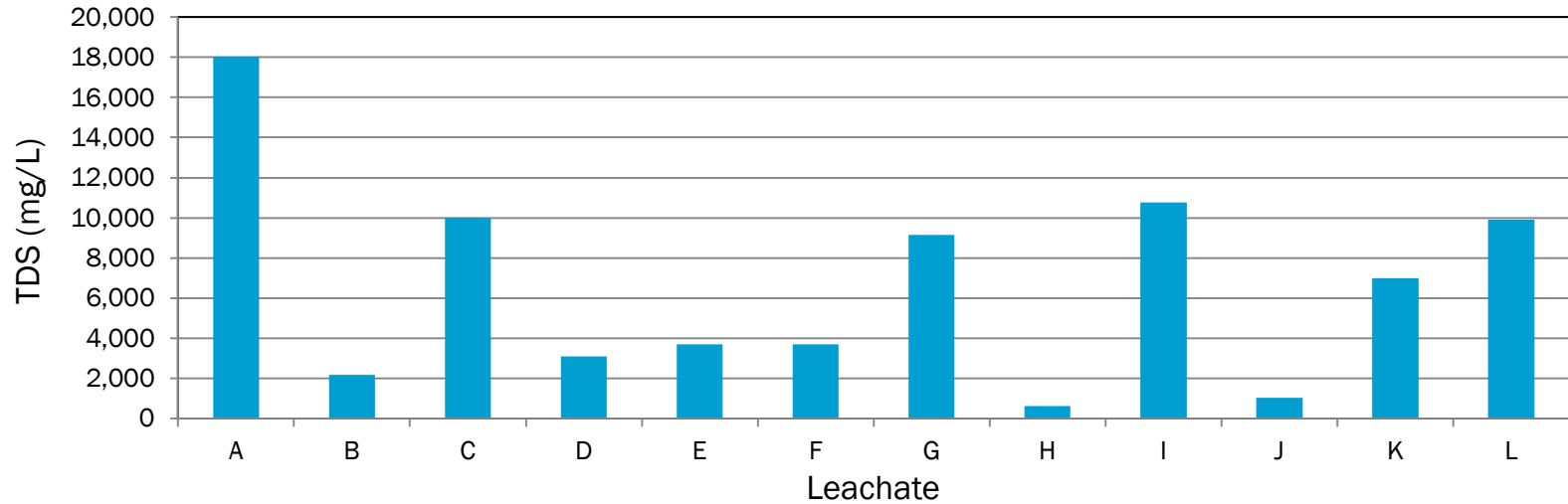
## Landfill B

- Concerns of Leachate Color impacting UV Performance at POTW
- Treatability
  - Chlorination: 95% Removal (currently adopted to meet Antrim discharge requirements)
  - PerOzone: 90%
  - Ozone: 86 %
  - Ozone and PAC: 80%
  - PAC: 75%
  - Coagulation: 68%
- No Relationship between Color and UV transmittance
- Leachate Flow > 1% of POTW impacted UV performance (< 63% transmittance needed for adequate disinfection)

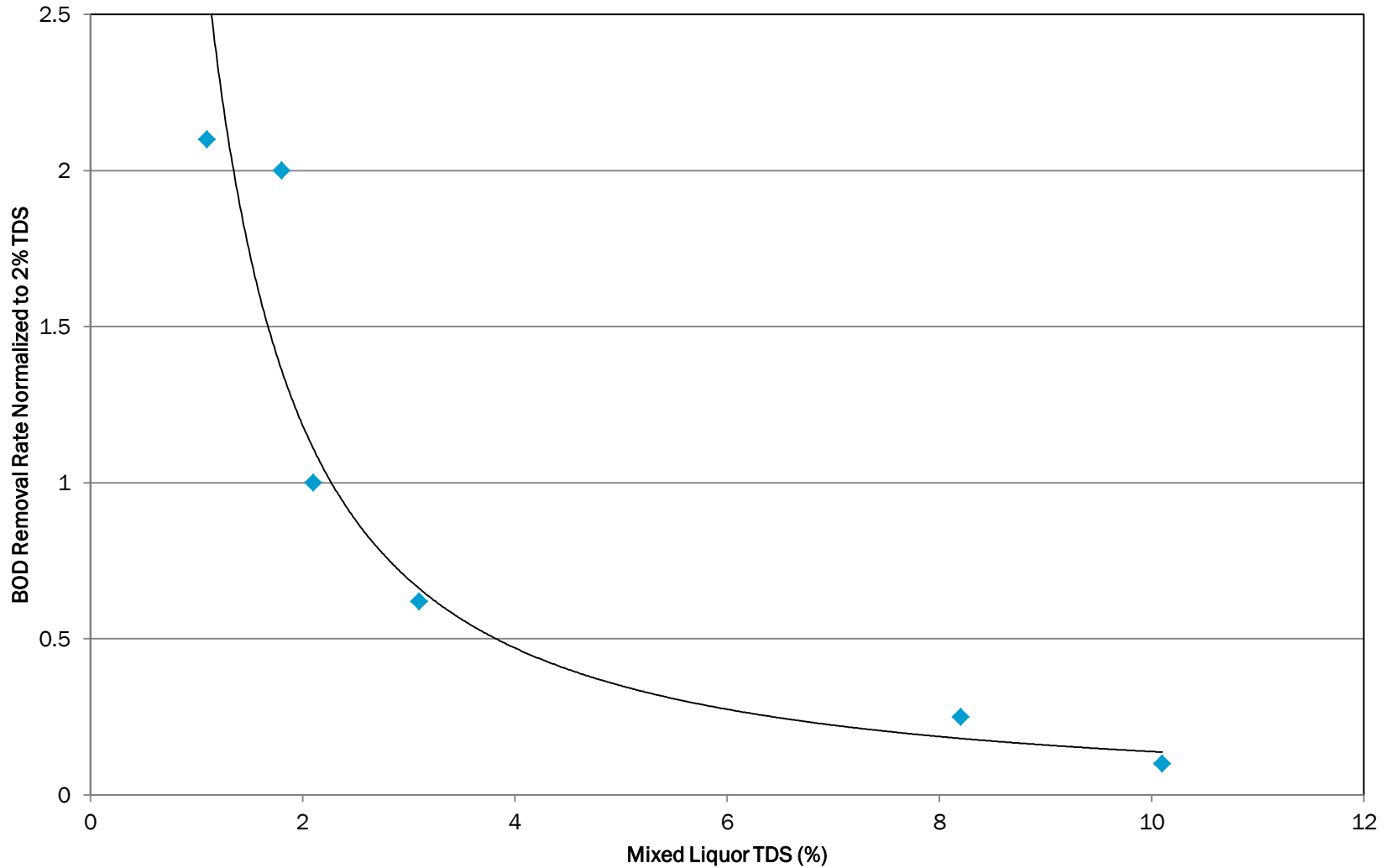
Technology	Removal (%)
Metals <sub>R</sub> /MBR	50
GAC	80.3
Ozone and GAC	82.3
PerOzone	89.7
RO	95.4

Color (PCU)	UV Transmittance (%)
900	0
105	0.2
100	0.1
50	0.1

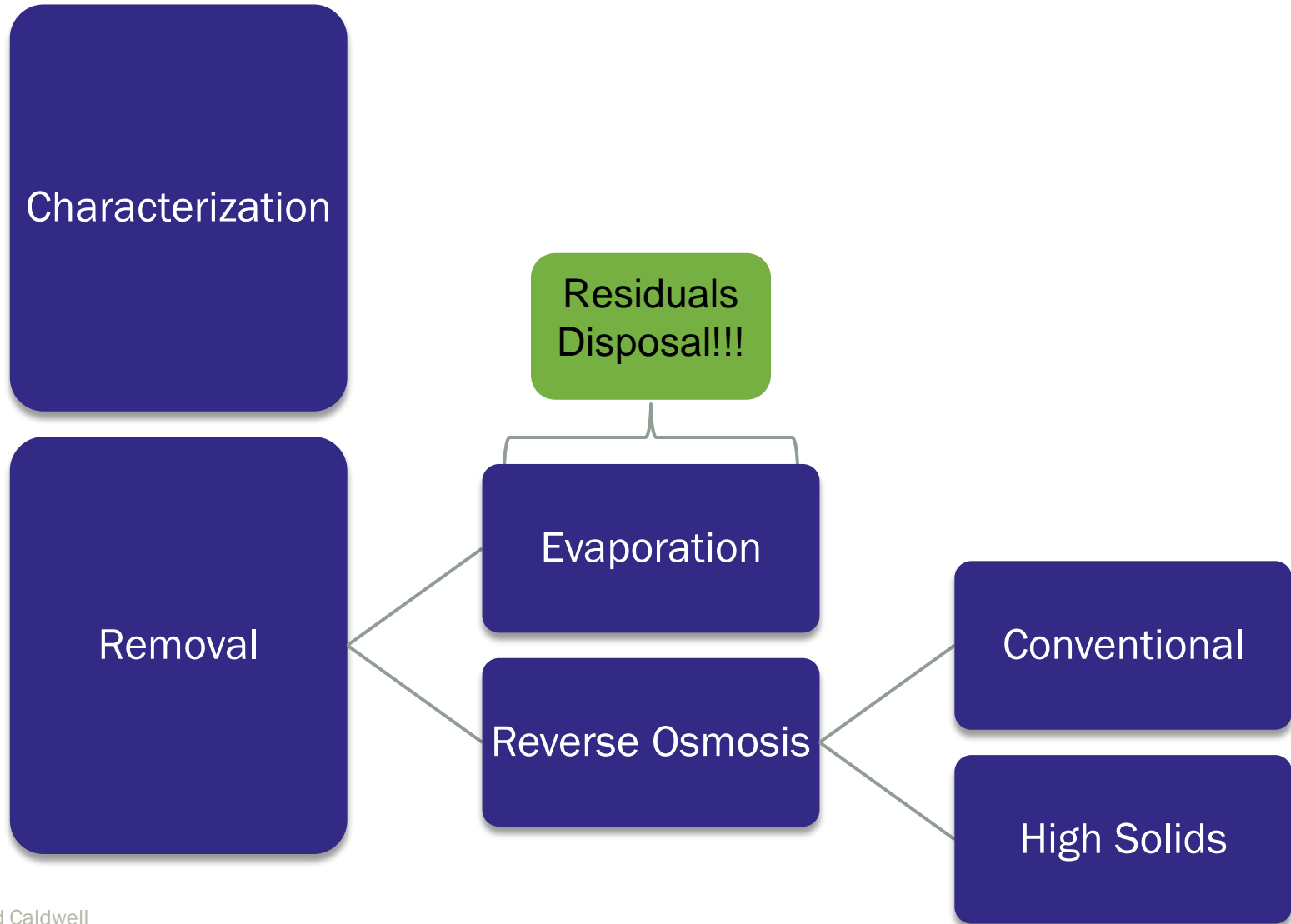
# TDS: Typical Range



# TDS: Effect on Organics Removal



# Inorganic TDS/Cl Removal



# Refractory Dissolved Organic Nitrogen - rDON

## What is rDON?

### Comprises of the following:

- Humic substances (humic acids, fulvic acids, and humins)
- Polymerized organic compounds
  - Endogenous decay of biomass and release of intracellular material
  - Released during high substrate utilization rate

# rDON Example

- Discharge to POTW which discharges to the Chesapeake Bay Watershed (CBW)
- rDON load to POTW:
  - 18% or 1.45 mg/L @ avg flow
  - 36% or 2.9 mg/L @ peak flow
  - POTW Discharge Allocation for TN = 8 mg/L
- Treatability: GAC, H<sub>2</sub>O<sub>2</sub>, Hypochlorite, and High pH were evaluated (no removal observed)
- Per CBW Program : variance could be achieved if the permittee can demonstrate that the constituent is not bioavailable in the plant and in the watershed (consistent with CBW models). Submit a preliminary design report identifying technologies and operational changes implemented

# Technologies on the Horizon

- Anaerobic treatment
- Nitrogen removal alternatives
  - Biological
  - Physical/chemical
- Contaminant specific sorbents
- Thermophilic (select wastes)



# Thank You!



**Environmental Research  
& Education Foundation**

*Lighting a path to sustainable waste management practices*

Kevin Torrens

201-574-4749

[ktorrens@brwnncald.com](mailto:ktorrens@brwnncald.com)

Brian Brazil

301-479-1263

[bbrazil@brwnncald.com](mailto:bbrazil@brwnncald.com)

EREF

[events@erefdn.org](mailto:events@erefdn.org)